

**IN THE SPECIFICATION:**

Please amend the paragraph on page 6, line 15, to page 7, line 21 as follows:

The present invention fluoropolymers can be prepared by radical polymerization in aqueous or organic solvent. The emulsion polymerization in aqueous medium is carried out in the presence of a water-soluble inorganic radical initiator, such for example a peroxide, a percarbonate, a persulphate or azo compounds. Generally said radicals have sufficiently long half-life times, such that said compounds are present during the whole polymerization. In some cases a reducing agent can be added so to make easier the initiator decomposition. Said compounds can for example be iron salts. The initiator amount depends on the reaction temperature and on the reaction conditions. In particular said polymers are synthesized at a temperature in the range 60°C - 90°C, preferably 70°C - 80°C. Besides for the synthesis of said copolymers in particular a chain transfer agent is introduced so to regulate the polymer molecular weight, giving narrow molecular weight distributions. The used transfer agents can be ethane, methane, propane, chloroform, etc. The polymerization in aqueous phase takes place in the presence of fluorinated surfactants such for example perfluoroalkylcarboxylic acid salts (for example ammonium perfluorocaprylate, ammonium perfluorooctanoate), or other compounds such for example perfluoroalkyoxybenzen perfluoroalkoxybenzene-sulphonic acid salts, as described for example in EP 184,459. For the invention copolymer synthesis it is particularly advantageous to

carry out the polymerization in aqueous phase in the presence of perfluoropolyethers, which can be added in the reaction medium under the form of aqueous emulsion in the presence of a suitable dispersing agent, as described in EP 247,379 or, preferably, in the form of aqueous microemulsion as described in USP 4,864,006.

Please amend the paragraph on page 15, lines 7-15, as follows:

The polymerization described in Example 1 is repeated except for the amount of the following components:

- ethane: 0.515 absolute bar ( $5.15 \times 10^4$ ) Pa;
- FMVE: 2.87 absolute bar ( $2.87 \times 10^5$ ) Pa;
- molar ratio TFE/FMVE in the fed monomeric mixture: 26.03;
- composition of the gaseous mixture present in the reactor head (analyzed by gas chromatography gas chromatography) before the reaction start, expressed in per cent percent by moles: TFE 82.5%, FMVE 16.0%, ethane 1.5%.